

## MARKED UP VERSION OF AMENDED CLAIMS

2. (Amended)      The [P] process [according to] of claim 1, wherein in step (a) the temperature is raised to a value of between 140-200°C.
3. (Amended)      The [P] process [according to] of claim 2, wherein in step (a) the temperature is raised to a value of between 160-200°C.
4. (Amended)      The [P] process [according to] of claim 3, wherein the temperature of the resulting mixture is raised from a value of between 120-150°C t o a value of between 160-180°C by making use of the indirect heat exchange means.
5. (Amended)      The [P] process [according to any one] of claim[s] 1[-4], wherein the pressure in step (b) is sufficiently high in order to obtain both phases in the liquid state.
6. (Amended)      The [P] process [according to] of claim 5, wherein in step (b) the liquid water phase has a pH of below 7.
7. (Amended)      The [P] process [according to] of claim 6, wherein the pH of the liquid water phase is between 4 and 6.
8. (Amended)      The [P] process [according to any one] of claim[s] 1[-7], wherein the starting emulsion has a water content of between 1-40% by weight, a surfactants content of between 0.01-5% by weight and an oil content of between 60-85% by weight, wherein the oil alone has a viscosity of above 305 Pa.s at 20°C.
9. (Amended)      The [G] gasification process for preparing synthesis gas, wherein a liquid bituminous oil is obtained according to the process [according to any one] of claim[s] 1[-8] and wherein said liquid bituminous oil, having a temperature of above 140°C, is fed to a gasification unit in which synthesis gas is obtained.

10. (Amended)      The [U] use of the oil phase obtained in the process [according to any one] of claim[s] 1[-9] having a temperature of above 140 °C as feedstock in a gasification process.

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